

Numerical study of effect of staggering the artificial roughness on heat transfer coefficient.

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Abstract— Use of artificial roughness on the absorber plate of solar air heater can significantly improve the performance of solar air heater. Arrangement of roughness element on the absorber plate also affects the performance of heat transfer. In this study an attempt is made to investigate the effect of staggering the roughness element on the amount of heat transfer coefficient. Steady states external forced convection heat transfer from artificially roughen absorber plate of solar air heater having spherical Elements is studied numerically. Ansys fluent software is used to develop a 3D numerical model for investigation of effect of staggering the artificial roughness element on the overall heat transfer coefficient. It is observed that average heat transfer coefficient reduces in comparison with the inline arrangement of roughness element.

Keywords—Absorber plate, solar air heater, Heat transfer coefficient, Staggered arrangement.

I. INTRODUCTION

Demand for energy is tremendously increasing due to fast growing population, industrialization and transportation needs. The fossil fuels are diminishing day by day because of their limited source worldwide. Therefore now it's a need of time to switch over to the non conventional energy sources. Solar air heaters are widely used for drying and space heating applications and usually have flat plate absorber plate for solar energy collection. However they generally exhibit low thermal performance owing to high thermal losses from absorber plate coupled with poor carrying capacity of the air, which is the working fluid. Hence there is need for the development of an efficient flat plate solar air heater. Various techniques have been proposed by the previous researchers for increased in thermal performance and are found to have different extents of heat transfer augmentation and corresponding pressure drop in the flow. Mr M S Aazad et al uses diagonally chamfered cuboids to generate roughness on absorber plate for Reynolds number ranging from 5000 to 22500 with constant heat flux of 1000 w/m^2 on absorber plate. He found out the highest value of enhancement ratio 1.54 at least Reynolds number with relative roughness pitch (transverse and longitudinal) of 7, relative roughness height of 0.088 and 12mm cube arm [1]. Mr. Manjunath M S studied the effect of spherical turbulence generators on thermal efficiency and thermo hydraulic performance of flat plate. Solar air heater for the Reynolds number range of 4000-25000. He found the maximum enhancement in Nusselt number is found to be 2.52 times higher as compared to the base model corresponding to the Reynolds number of 23560 and relative roughness pitch of 3[2]. Chandra Prakash et al carried out an experimental investigation on heat and fluid flow characteristics of solar air heater duct having spherical and inclined protrusions in the Reynolds number ranging from 2000 to 20000. HE found out that the Maximum thermo-hydraulic performance parameter is 3.66, for r/g value of 0.8, P/e value of 25 and Pr/P value of 0.5[3]. R.S. Gill et al did an experimental investigation on heat transfer and friction factor characteristics of solar air heater duct roughen with broken arc rib combined with staggered rib piece in the Reynolds number ranging from 2000 to 16000. He conclude that the thermo-hydraulic performance of broken arc rib geometry is better in comparison to roughness geometries reported in literature having staggered rib piece due to lesser frictional losses[4]. In the studied literature very little work is found on the staggered arrangement of the roughness elements on the absorber plate of the solar air heater. So here in this work the objective is to find out the effect of effect of staggering the spherical roughness elements on the absorber plate of solar air heater.

II. MATERIALS & METHODS

The test section has a length of 1200mm and is fixed with an absorber plate at the top. The design parameters that could influence the thermal performance are the size and span wise distribution of the turbulators. The diameter (D) of the sphere is as 25mm while the relative roughness pitch (P/D) is taken as 3 which are mentioned as best case by author M.S. Manjunath et.al[2]. The transverse pitch is fixed at 37.5mm for all the cases with spherical turbulators. Grid independence test (optimum mesh) In order obtain the better result better mesh is required together with computational time is important concern here. Hence a simulation is carried out at a mass flow rate of 0.014kg/s which corresponds to a Reynolds number of about 8200 [2].

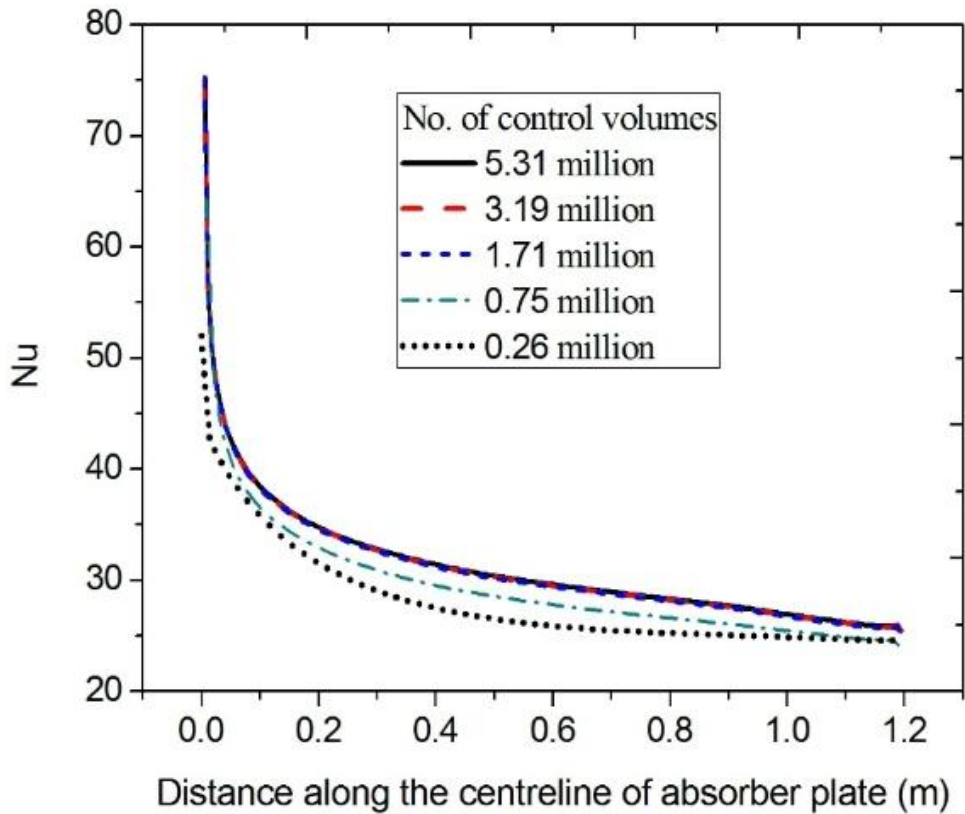


Figure 1[2]

The simulation is carried out at a mass flow rate of 0.014kg/s which corresponds to a Reynolds number of about 8200. The number of elements prepared is 1366509 which is kept closer to the best cell density specified.

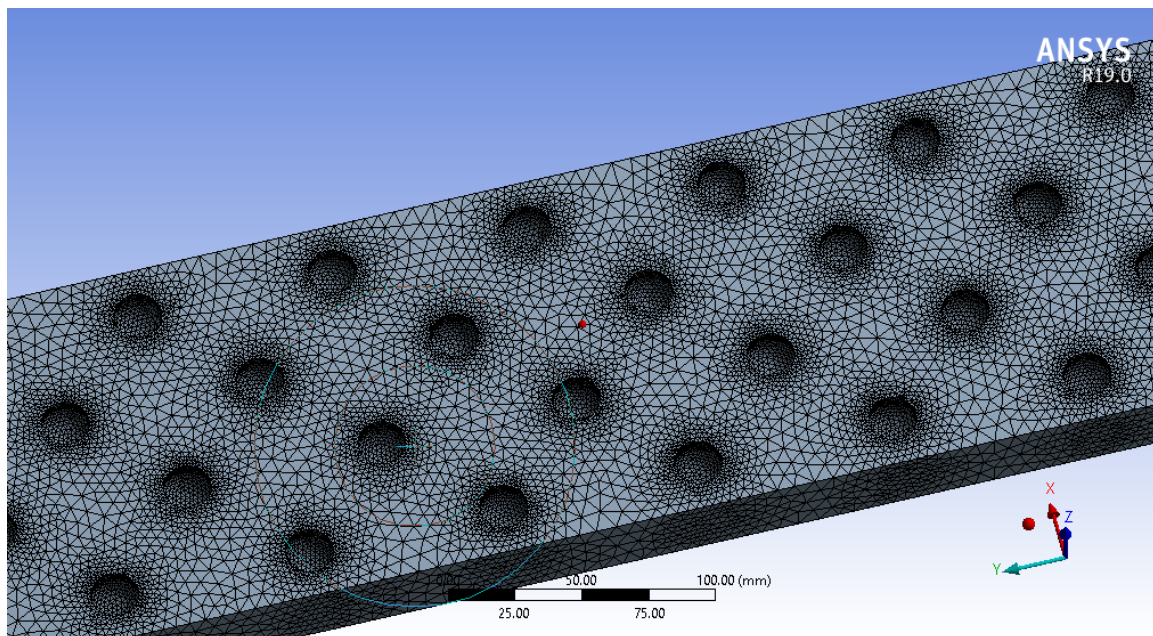


Figure 2

The meshing quality overall is found to be good to begin the CFD analysis in fluent. Boundary Conditions are At duct inlet the mass flow rate is given as 0.004 kg/s (kept at 300 K), At duct outlet the backflow reference pressure is taken as absolute pressure and the gauge pressure is given as 101325 Pa (kept at 300 K), At the top surface of absorber plate the heat flux is applied as 1084 W/m² which is recorded as Solar radiation heat flux applied through solar load model at a longitude of 74.7860E, latitude13.3430N and GMT of

+5.5 is used in the solar load model to define the global position of Manipal for 1st of April at 12 noon conditions. The rest of the three walls are considered as smooth walls kept at 300 K with No-Slip impermeable wall condition. Also, to reduce the size of domain and to save the computational time the planar wall symmetry condition is applied. Fluent with double precision pressure based CFD solver is used for numerical simulation. The pressure velocity coupling is done using SIMPLE scheme segregated solver. The SIMPLE algorithm uses a relationship between velocity and pressure corrections to enforce mass conservation and to obtain the pressure field. In Spatial discretization Body-force weighted scheme is used for pressure while momentum, turbulence kinetic energy and specific dissipation rate is carried out using second order upwind scheme. The convergence of the solution is considered when the residuals in the computation domain fall below 10^{-6} for energy and 10^{-5} for momentum and Continuity equations. Besides the residuals, surface monitors for the temperature of air at duct outlet and absorber plate temperature are also used to confirm the convergence of the solution. The thermo-physical properties of air such as density, dynamic viscosity and thermal conductivity are considered to be function of temperature and are evaluated from the following equations.

$$\rho = 3.9147 - 0.016082 T + 0.016082 T + 2.9013 \times 10^{-5} T^2 - 1.9407 \times 10^{-8} T^3.$$

$$\mu = (1.6157 + 0.06523T - 3.0297 \times 10^{-5} T^2) \times 10^{-6}$$

$$K = (0.0015215 + 0.097459T - 3.3322 \times 10^{-5} T^2) \times 10^{-3}$$

Where Density came out to be 1.177372 kg/m^3 and Viscosity is $1.845797 \times 10^{-5} \text{ Kg/m-s}$ and the thermal conductivity is $0.0262393115 \text{ W/m-K}$.

Selection of Turbulence Model

The CFD software used for the analysis offers various turbulence models such as Standard k-ε model, Renormalization Group (RNG) k-ε model, Realizable k-ε model, standard k-ω model and Shear Stress Transport (SST) k- ω model for fluid flow and heat transfer studies. The simulation is carried out using each of these turbulence models and the values of Nusselt number (Nu) for heat transfer from absorber plate to duct air stream at different Reynolds number of the flow are plotted as shown in Fig. From Fig. it is observed that the results of SST k-ω model closely matches with that of Dittus-Boelter equation.

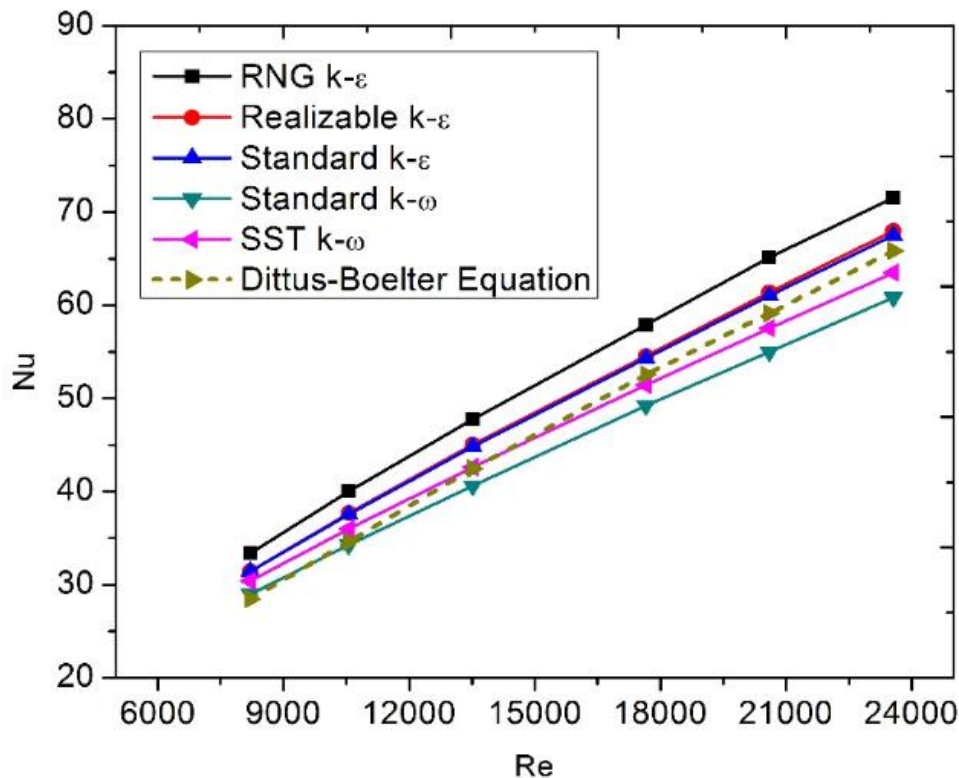


Figure 3 Selection of turbulence model for the CFD analysis. [2]

Also according to fluent shear-stress transport (SST) K-ω models has few specific turbulence features such as gradual change from the standard K-ω model in the inner region of the boundary layer to a high-Reynolds-number version of the K-ε model in the outer part of the boundary layer and modified turbulent

viscosity formulation to account for the transport effects of the principal turbulent shear stress. Hence the whole CFD analysis is carried out based on the $k-\omega$ model with energy equations were on.

III. RESULTS AND DISCUSSION

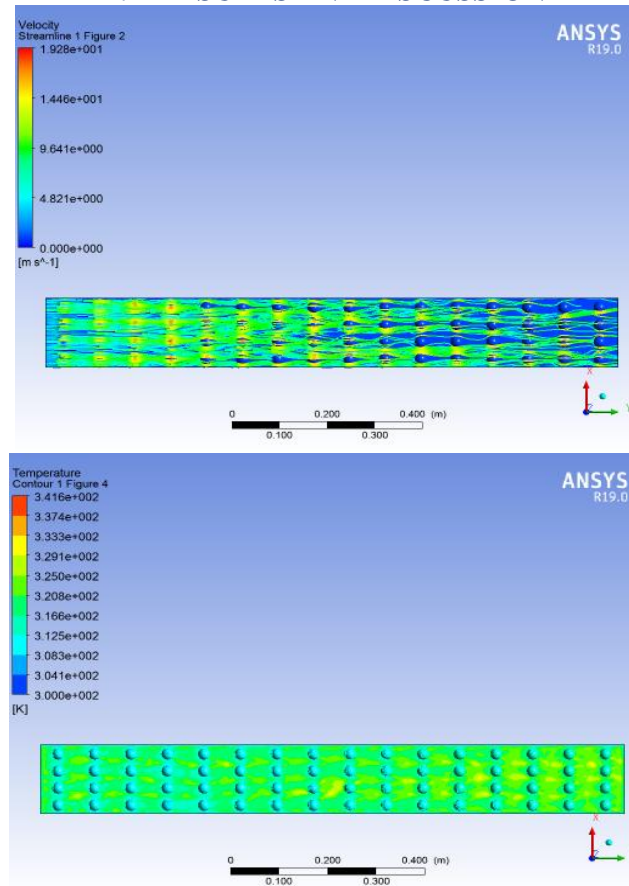


Figure 4 the velocity and temperature plots for the unstaggered arrangement of elements

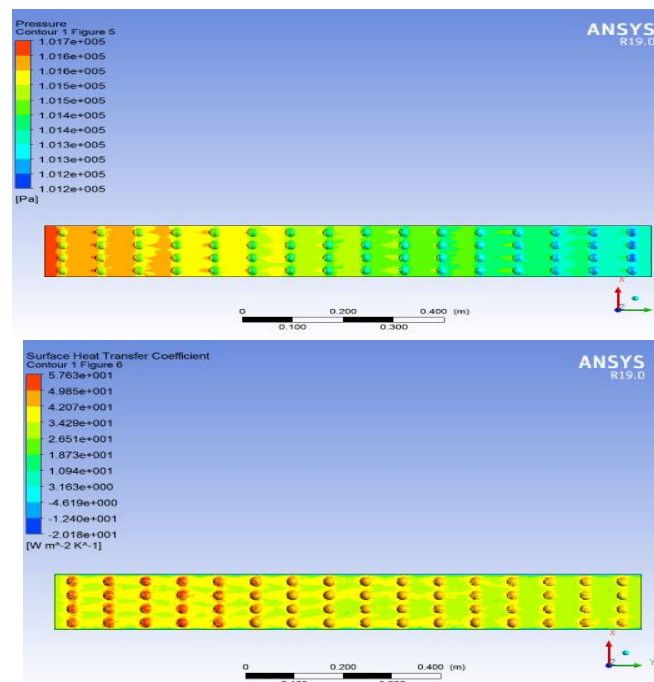


Figure 5 The Pressure and Surface heat transfer coefficient plots for the unstaggered arrangement of elements.

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In the inline arrangement of spherical roughness elements average heat transfer coefficient and nusselt no is found to be 38.82 and 78.04 respectively.

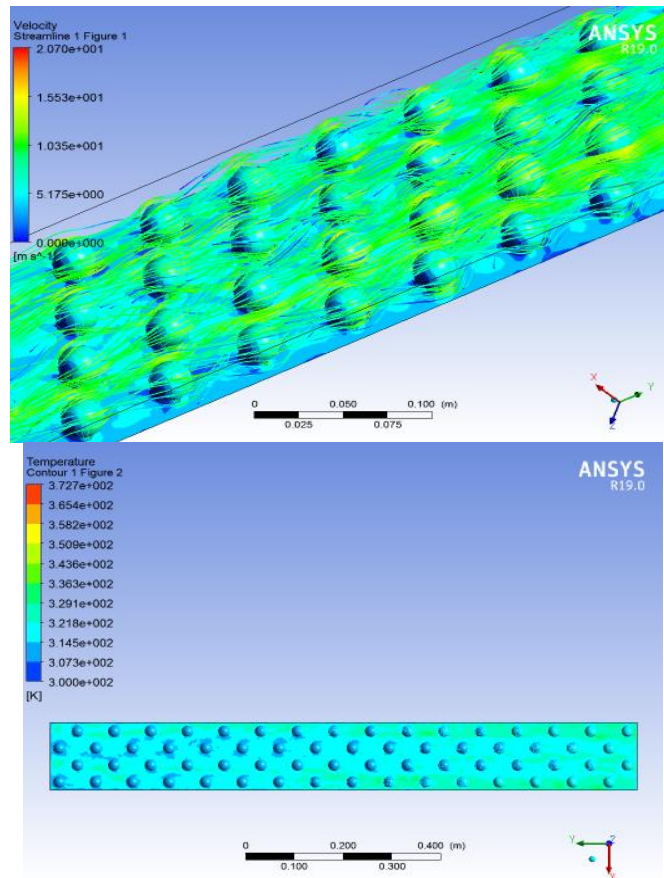


Figure 6 The velocity and temperature plots for the staggered arrangement of elements

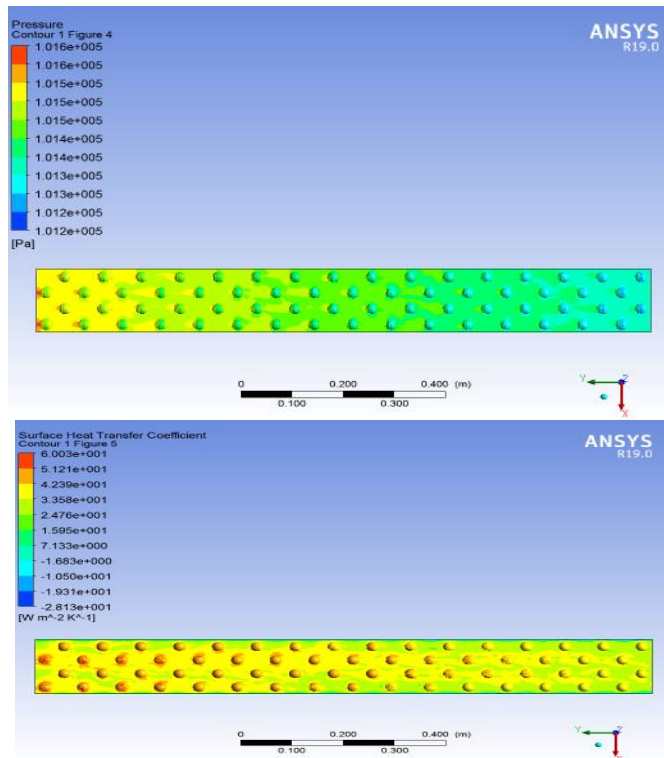


Figure 7 The Pressure and Surface heat transfer coefficient plots for the staggered arrangement of elements.

In the staggered arrangement of spherical roughness elements the average heat transfer coefficient and nusselt number is found to be 37.93 and 72.31 respectively.

IV. CONCLUSION

A three dimensional CFD analysis is carried out to evaluate the effect staggering the spherical turbulence elements on heat transfer enhancement of flat plate solar air heater. The analysis shows that the average heat transfer coefficient decreases by 2.3% as compared to the inline arrangement of the roughness elements.

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